

Siprem International srl

Continuous Membrane Press

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Contrinuous Membrane Press

The new generation of machines able to both load product and unload marcs in continuous operation.

(European Patent no. 0 569 695 on 20th November 1996)









The tank is fixed to the chassis by means of two supports with bronze bushes, which allows it to rotate by means of a gearbox. The chassis is made of carbon steel and all the parts in contact with the product are made of Stainless Steel Aisi 304.





The tank contains several diaphragms inside it, basically semi-elliptical in shape, and arranged in such a way as to create first free dejuicing chamber and a series of "pressure chambers", each with its own specific function.







The tank has a large perforated surface area with holes that are flared outwards and is self-cleaning to ensure efficient dejuicing and a de-blocking action on the sections where the juice passes through.

The dejuicing holes take up the entire external surface of the free dejuicing chamber, whilst in the remaining pressure chambers only half of the circumference is perforated.

Working principle



The dejuicing chamber is located at one end of the cylinder, where the product is fed continuously by means of an axial filling conduit. This chamber is designed so that it drains completely and guarantees the extraction of a high percentage of free-run juice during the filling phase.





Working principle

The various pressure chambers are separated from each other. Inside which the product is gradually subjected to increased pressure as it progresses towards the final chamber. This process makes it possible to achieve the same effect as in a traditional membrane press using a system involving different phases, each one with different pressures.





Working principle

Each compression chamber contains a separate (from the other chambers) press membrane. The membrane that separates the two tank sections consists of a nylon fabric, coated with a food grade non-toxic material. The fabric can be heat welded if any repairs are necessary.

A pneumatically operated automatic door allows the intermittant discharge of the exhausted marc from the final pressure chamber.







Working principle

A system of pressurised fluid introduction is also present, consisting of a collector and a series of inlets, controlled by respective valves, for the different pressure chambers.



Working principle



The various pressing phases are interspersed by crumbling to allow continual renewal of the grape mass structure achieving excellent dejuicing rates and to move forward the pomace from one chamber to the next one

Example of operating pressure setting

Chamber 1	0,20 bar
Chamber 2	0,40 bar
Chamber 3	0,80 bar
Chamber 4	1,20 bar
Chamber 5	1,50 bar
Chamber 6	1,80 bar
Chamber 7	2,00 bar

N.B. – The number of chamber spans from 6 to 7 according to the specific model

Working principle

The juice obtained by the processing is collected in different troughs, located under the press, allowing separation at every stage.

I TROUGH	40%
II TROUGH	20%
III TROUGH	15%
IV TROUGI	12%
V TROUGI	8%
VI TROUGI	5%

N.B. – The above indicated percentages refer to total yield of 76-80 %

Overall dimensions (expressed in mm)







MISU	RE D'IN	GOMBRO	E PESO				
PCM100	12780	2300	3400	900	1050	2300	8700 kg
PCM200	14657	2600	3450	1050	1200	2400	9500 kg
PCM400	16644	3300	4150	1050	1200	2400	13000 kg
	Α	В	С	D	E	F	PESO

Le quote sono espresse in millimetri. La Ditta costruttrice si riserva il diritto di apportare alle macchine le modifiche necessarie per il loro miglioramento; per tali motivi i dati hanno valore indicativo.





PCM100	220hl	6	10-16 tonn	13-22 tonn	9,2kW	13kW	2 kW	120 mm	80-100 mm	740 mm	potenza di 22kW portata elaborata 3000 l/min a 1 Mpa (10 bar) 1 serbatoio di accumulo da 5000 litri a 1 Mpa (10 bar)
PCM200	350hl	6	18-25 tonn	25-33 tonn	15kW	2x13kW	2 kW	120 mm	80-120 mm	740 mm	potenza di 30kW portata elaborata 4500 l/min a 1 Mpa (10 bar) 2 serbatoi di accumulo da 3000 litri a 1 Mpa (10 bar)
PCM400	640hl	7	32-45 tonn	42-60 tonn	18kW	2x13kW	2 kW	120 mm	80-120 mm	740 mm	potenza di 45kW portata elaborata 6000 l/min a 1 Mpa (10 bar) 2 serbatoi di accumulo da 5000 litri a 1 Mpa (10 bar)
	capacità del serbatoio a vuoto	numero di camere di pressatura	produzione oraria di uva fresca, pigiata o diraspata	produzione di uva fermentata, espressa come uva iniziale svinata	potenza del motore di rotazione	potenza di ciascuna della soffiante	potenza del motore di rotazione dell'elica, dove previsto	diametro nominale del condotto di carico	diametro nominale dei condotti delle tramogge di scarico del mosto	diametro del portello di evacuazione della vinaccia	caratteristiche del compressore

Technical data



Advantiages of the Continuous System

- High output capacity guaranteed by the continuous cycle operation

- Soft and calibrated pressing, a typical feature of membrane operation

- Fractional juice separation obtained through progressive regulation of working pressures

- Complete juice extraction from marcs ensured by the pressing technique.

Advantages of the continuous system compared with the discontinuous one

PCM

- -Continuous operation
- -Product quality similar to that obtained by traditional membrane presses of the same kind.
- -High juice yield.
- -Working cycle duration: about 1 hour/1 hour and 20' (from the charging to the discharging of the exhausted marcs).
- Possibility of separating the juice at every different pressure stage.
- Low working pressure.
- Complete automation of the various operations
- Extremely versatile, able to adapt to the various types of grape.
- Easily swapped from one type of grape to another.
- Automated and efficient washing operations
- -Strong reliability due to the use of established technology used for over a decade.

Discontinuous System

- Discontinuous processing cycle.
- The pressing cycle depends on the product being processed and the size of the press can take over 2 hours
- Higher installation costs



Control Panel

Modern and functional, immediately understood by means of the symbols used. Equipped with a PLC for programming, the control panel allows the operator to set the various working phases of the machine, to edit the parameters and to check correct machine function by digital keyboard display.

The operator can program:

- -pressure level in each pressing chamber with a maximum difference of 0.4 bar between 2 contigue chamber
- -the holding time: is the same for each chamber
- -the number of revolutions of the tank between two pressing cycles (necessary for cake breaking and pomace forwarding)
- -the number of revolution of the tank with open door (necessary to discharge the pomace of the last pressure chamber)





Pneumatic circuit

The machine's substantial need of compressed air is supplied by a rationally designed system that includes blowers, stainless steel pipes, pressure reducers, safety and exchange valves and discharged silencers.

Everything is controlled by its own control panel.





Unloading door

The device, with pneumatically controlled automatic opening, allows the aperture through which the marcs is released to be opened either completely or only partially (according to the working capacity of the external marc removal device).







Standard Axial type



Axial screwed type





"Manhole Door"

For easy membrane inspection





Automatic Washing

The procedure, entirely PLC controlled, is carried out using a series of suitably located spray nozzles which spray the surfaces to be cleaned with water from the mains supply.





Juice Collecting Troughs

The trough underneath the static draining chamber is bigger than the troughs under the pressing chambers.



Features of the Working cycle

Juice drainage

This is performed continuously at every pressure stage through the side of the pressing chamber, equipped with suitably shaped openings. In this way juice with different characteristics can be drained separately.



Features of the Working cycle

Pomace discharging

The processing residue, completely strained of juice, is unloaded from the machine on the opposite end to the feed, via the tank's rotational movement.



Some analysis of the juice/wine obtained Prosecco juice vintage 2002 analysis-Winery: Cantina sociale Ormelle, Treviso

PRECHAMBER N.1			PRECHAMBER N.3		
Reducing sugar	%w/v	15,8	Reducing sugar	%w/v	15,86
pH (electrometric method)		3,5	pH (electrometric method)		3,54
Potassium	g/l	1,88	Potassium	g/l	1,95
Tartaric Acid	g/l	5,67	Tartaric Acid	g/l	5,79
Titratable Acidity (expressed in tartaric acid)	g/l	7,2	Titratable Acidity (expressed in tartaric acid)	g/l	7
Total sulpur dioxide	mg/l	34	Total sulpur dioxide	mg/l	35
Malic Acid (-)	g/l	4,94	Malic Acid (-)	g/l	4,61
Total Polyphenols (uv) expressed in galic acid	mg/l	193	Total Polyphenols (uv) expressed in galic acid	mg/l	213
Suspended solids (centrifugation)	%	1,74	Suspended solids (centrifugation)	%	0
Assimilable nitrogen	mg/l	184	Assimilable nitrogen	mg/l	186
PRECHAMBER N.2			PRECHAMBER N.4		
Reducing sugar	%w/v	15,62	Reducing sugar	%w/v	15,71
pH (electrometric method)		3,53	pH (electrometric method)		3,61
Potassium	g/l	1,91	Potassium	g/l	2,1
Tartaric Acid	g/l	5,81	Tartaric Acid	g/l	6,04
Titratable Acidity (expressed in tartaric acid)	g/l	7,1	Titratable Acidity (expressed in tartaric acid)	g/l	7,3
Total sulpur dioxide	mg/l	38	Total sulpur dioxide	mg/l	35
Malic Acid (-)	g/l	4,68	Malic Acid (-)	g/l	5,16
Total Polyphenols (uv) expressed in galic acid	mg/l	203	Total Polyphenols (uv) expressed in galic acid	mg/l	222
Suspended solids (centrifugation)	%	0,67	Suspended solids (centrifugation)	%	0,62
	mall	470	Analmilahla nitranan	ma/l	100





		PRECHAMBER N.6		
%w/v	15,66	Reducing sugar	%w/v	14,9
	3,59	pH (electrometric method)		3,72
g/l	2,13	Potassium	g/l	2,47
g/l	5,98	Tartaric Acid	g/l	5,46
g/l	7,3	Titratable Acidity (expressed in tartaric acid)	g/l	7
mg/l	36	Total sulpur dioxide	mg/l	41
g/l	5,09	Malic Acid (-)	g/l	5,84
mg/l	221	Total Polyphenols (uv) expressed in galic acid	mg/l	294
%	0,78	Suspended solids (centrifugation)	%	0,45
mg/l	190	Assimilable nitrogen	mg/l	195
	%w/v g/l g/l mg/l g/l mg/l % mg/l	%w/v 15,66 3,59 g/l 2,13 g/l 5,98 g/l 7,3 mg/l 36 g/l 5,09 mg/l 221 % 0,78 mg/l 190	%w/v15,66PRECHAMBER N.6%w/v15,66Reducing sugar3,59pH (electrometric method)g/l2,13Potassiumg/l5,98Tartaric Acidg/l7,3Titratable Acidity (expressed in tartaric acid)mg/l36Total sulpur dioxideg/l5,09Malic Acid (-)mg/l221Total Polyphenols (uv) expressed in galic acid%0,78Suspended solids (centrifugation)mg/l190Assimilable nitrogen	%w/v15,66PRECHAMBER N.6%w/v3,59pH (electrometric method)%w/vg/l2,13Potassiumg/lg/l5,98Tartaric Acidg/lg/l7,3Titratable Acidity (expressed in tartaric acid)g/lg/l36Total sulpur dioxidemg/lg/l5,09Malic Acid (-)g/lmg/l221Total Polyphenols (uv) expressed in galic acidmg/l%0,78Suspended solids (centrifugation)%mg/l190Assimilable nitrogenmg/l

Laboratory Michelet (Treviso)

Sangiovese juice vintage 2002 analysis – Winery: Cantine soc. Chianti Senesi e Fiorentini (Siena)

PRECHAMBER NO.1			PRECHAMBER NO. 3		
Total acidity in tartaric acid	gr/l	8	Total acidity in tartaric acid	gr/l	9,1
pH (electrometric method)		3,2	pH (electrometric method)		3,3
Total sulphur dioxide	mg/l	60	Total sulphur dioxide	mg/l	70
Total Polyphenols	mg/l	1.632,00	Total Polyphenols	mg/l	1.930,00
Malic Acid (-)	gr/l	2,5	Malic Acid (-)	gr/l	2,61
Tartaric Acid	gr/l	1,83	Tartaric Acid	gr/l	1,91
Potassium	mg/l	750	Potassium	mg/l	802
Assimilable Nitrogen	mg/l	123,2	Assimilable Nitrogen	mg/l	169,4
Brix Sugars	gr/l	8,93	Brix Sugars	gr/l	9,55
Suspended solids	gr/l	29	Suspended solids	gr/l	27
PRECHAMBER NO. 2					
PRECHAMBER NO. 2 Total acidity in tartaric acid	gr/l	9,5			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method)	gr/l	9,5 3,25			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide	gr/l mg/l	9,5 3,25 72			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols	gr/l mg/l mg/l	9,5 3,25 72 1.873,00			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-)	gr/l mg/l mg/l gr/l	9,5 3,25 72 1.873,00 2,69			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-) Tartaric Acid	gr/l mg/l mg/l gr/l gr/l	9,5 3,25 72 1.873,00 2,69 2,09			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-) Tartaric Acid Potassium	gr/l mg/l mg/l gr/l gr/l mg/l	9,5 3,25 72 1.873,00 2,69 2,09 800			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-) Tartaric Acid Potassium Assimilable Nitrogen	gr/l mg/l mg/l gr/l gr/l mg/l mg/l	9,5 3,25 72 1.873,00 2,69 2,09 800 168			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-) Tartaric Acid Potassium Assimilable Nitrogen Brix Sugars	gr/l mg/l mg/l gr/l gr/l mg/l gr/l	9,5 3,25 72 1.873,00 2,69 2,09 800 168 9,52			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-) Tartaric Acid Potassium Assimilable Nitrogen Brix Sugars Suspended solids	gr/l mg/l gr/l gr/l mg/l mg/l gr/l gr/l	9,5 3,25 72 1.873,00 2,69 2,09 800 168 9,52 25			
PRECHAMBER NO. 2 Total acidity in tartaric acid pH (electrometric method) Total sulphur dioxide Total Polyphenols Malic Acid (-) Tartaric Acid Potassium Assimilable Nitrogen Brix Sugars Suspended solids	gr/l mg/l gr/l gr/l mg/l gr/l gr/l	9,5 3,25 72 1.873,00 2,69 2,09 800 168 9,52 25			

Laboratory Imavi (Ancona)

Sangiovese juice vintage 2002 analysis – Winery: Cantine soc. Chianti Senesi e Fiorentini (Siena)





Poggibonsi (SI)

Lanciano (CH)

Faenza (RA)

Faenza (RA)

Montespertoli (FI)

Castelfranco Emilia (MO)

<u>Mod</u>	PCM	200

-VINI CHIANTI SENESI -COLLI FIORENTINI -C. S. MADONNA DEL CARMINE -Cantine RIUNITE & CIV S.c.a. -Cantina di FAENZA Soc. Agr. Coop. -Cantina dei COLLI ROMAGNOLI

Mod PCM 400

-C. S. di MONTEFORTE D'ALPONE -C. S. COPA -C.S. di ORSAGO -SOCIETA' INTESA -LE ROMAGNOLE S.c.a -Le ROMAGNOLE S.c.a. -Le ROMAGNOLE S.c.a. -C. S. di CERVETERI -CIV & CIV -C. S. UVAM -CASARSA LA DELIZIA -CANTINA TOLLO Soc. Coop Arl. -SAN MICHELE VIT. Coop. Agr. -CANTINA EUROPA -LIMIDI Soliera e Sozzigalli C. S. -AGRINTESA Soc. Coop. Agricola -VAGLIE AZ, AGR, Di Lumini A,

Verona (VR) n° 2 Faenza (RA) Treviso Bagnacavallo (RA) Alfonsine (RA) n°2 Fusianano (RA) Bagnacavallo (RA) Roma (RO) n° 2 Castelfranco Emilia (MO) Marsala (TP) Pordenone n°2 Tollo (CH) Minervino Murge (BT) Petrosino (TP) Limidi di Soliera (MO) Faenza (RA) n°2 Orvieto (TR)

White grapes White grapes White grapes White grapes White/red grapes White/red grapes White grapes White grapes White grapes White grapes White/red grapes White/red grapes White/red grapes White/red grapes Red grapes White grapes White grapes

Red arapes

Red arapes

White grapes

White/red grapes

White/red grapes

White/red grapes

PCM in the WORLD Mod PCM 100 -VINTECH PACIFIC New Zealand White grapes Mod PCM 200 -AD PLANTAZE Podgorica (Montenegro) White/red grapes -S. C. DEL CAMPO LA UNIÓN AB Albacete (Spagna) White/red grapes -VINICOLA MIOLO Ltda. White/red Bento Gonçalves (Brasile) grapes -VINARSKA "ARGEADI" dooel Gradsko (Macedonia) Red grapes Mod PCM 400 -C.S. di NEMEA Korinthiaki (Grecia) White/red Grapes -TITTAKIS Nikos Creta (Grecia) White grapes -COOP. PEZON Creta (Grecia) White grapes -PATRAS "PATRAIKI" Union Agr. Coop Patrasso (Grecia) White grapes SKopje (Macedonia) -FERSPED SKOVIN White grapes Alcazar de S. Juan (Spagna) -BODEGAS CONUVA SA White grapes -VINCOR INTERNATIONAL Niagara Falls, Ontario (Canada) White/red grapes

Some information from customer Vincor (Canada)



Overall with small exceptions on percentage of solids the SIPREM performance targets are met.

Please find below a couple of graphs with tons per hour averages 1 to 2 weeks prior to the end of harvest or after the first 12,000 T of grapes received.

As you will notice the percentage of solids are bit on a higher side, which in my opinion is attributed partially to the use of the de-juicer during pre feeding stage.

Currently we are working on redirecting the fresh grapes feed lines directly to SIPREM feeding hopper bypassing the de-juicer.

Note that the tons per hour averages include the CIP time at the end of run day as well as the pre-loading time.

I have to say that we are impressed by the ton per hour efficiency of the machine.

Kind Regards, Vincor









Click for YouTube video



Presentation context

- This presentation was given as part of a workshop on grape and juice processing equipment convened by the Australian Wine Research Institute (AWRI) at the 15th Australian Wine Industry Technical Conference in July 2013.
- The main intention of the workshop was to provide attendees with information on equipment that is new or unusual or that has not been widely used in Australia.
- This and the other presentations given were prepared by equipment suppliers, not by AWRI, and AWRI does not necessarily endorse the views presented. Before the purchase of any major winery equipment, AWRI recommends appropriate background investigations being undertaken; including visits to facilities already using similar equipment, consultation with independent experts and the performing of in-house trials.
- AWRI received no payment from suppliers for the inclusion of their equipment in the workshop.
- For any further details on the workshop please contact AWRI Senior Engineer, Dr Simon Nordestgaard, by email at <u>simon.nordestgaard@awri.com.au</u>.